

Dans le cadre de la
Formation « Hydraulique Fondamentale »
Unité de Formation pour la Performance Industrielle



en collaboration avec l'INP-ENSEEIH

Olivier THUAL
Toulouse INP
ENSEEIH



Chapitre 7 Ouvertures

OLIVIER THUAL
HYDRAULIQUE
POUR L'INGÉNIEUR GÉNÉRALISTE



Cépaduès
ÉDITIONS

15. Orifices et ajutages

$$Q = \mu A \sqrt{2 g h}$$



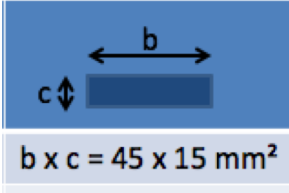
Ø = 16 mm

Ø = 22 mm

Ø = 31 mm

Ø = 42 mm

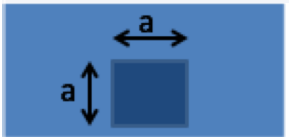
Ø = 60 mm



$b \times c = 45 \times 15 \text{ mm}^2$

$b \times c = 65 \times 21 \text{ mm}^2$

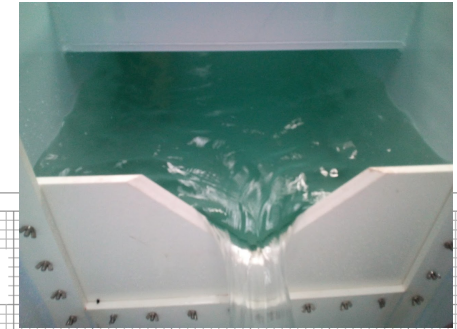
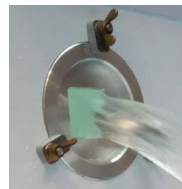
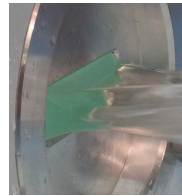
$b \times c = 92 \times 30 \text{ mm}^2$



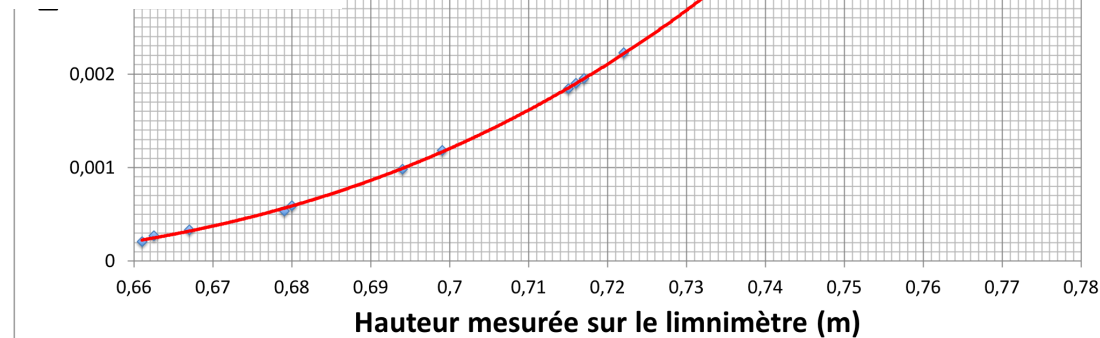
$a = 26 \text{ mm}$

$a = 37 \text{ mm}$

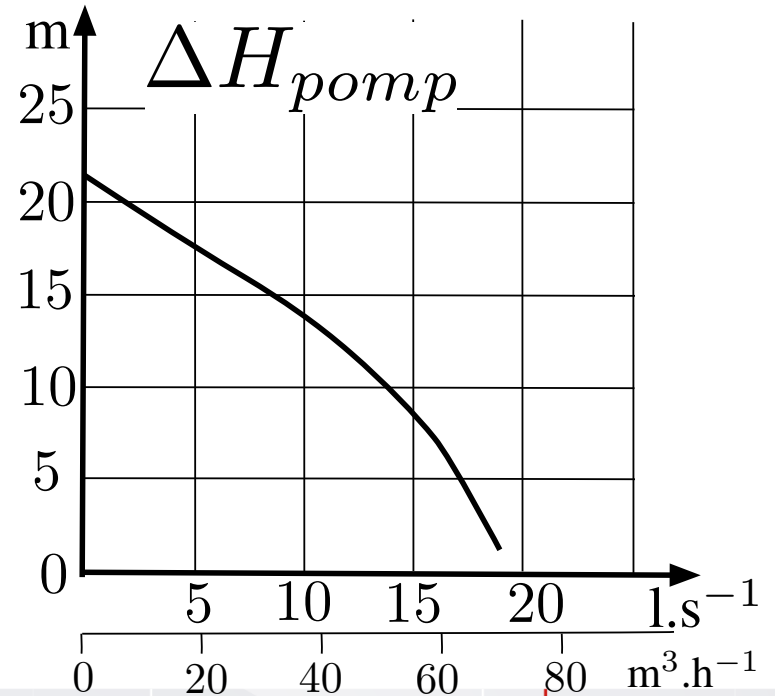
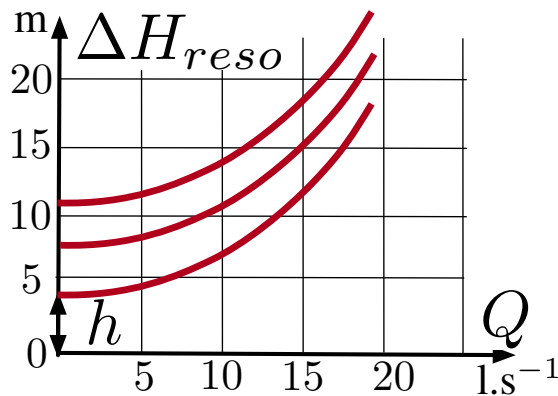
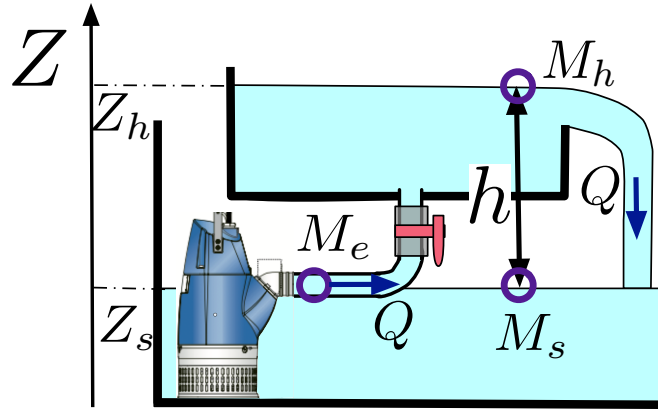
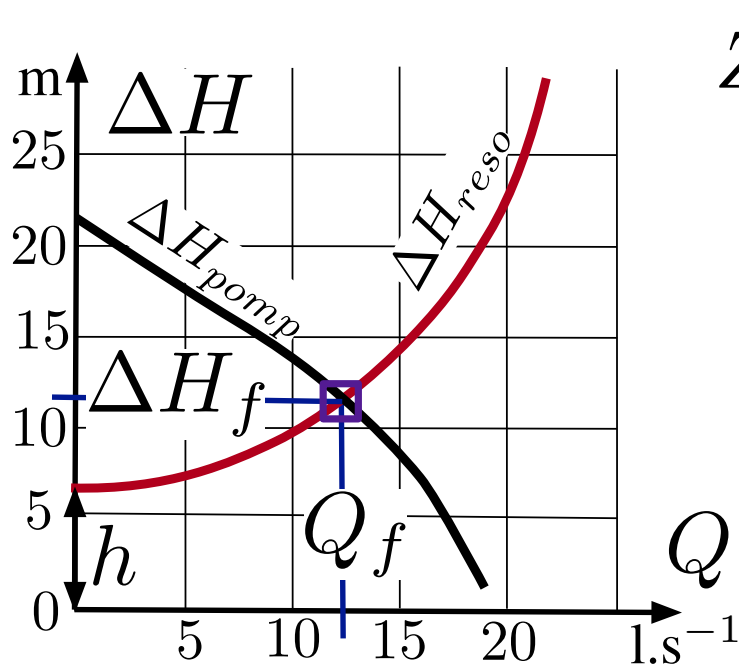
$a = 53 \text{ mm}$



Seuil 0,5

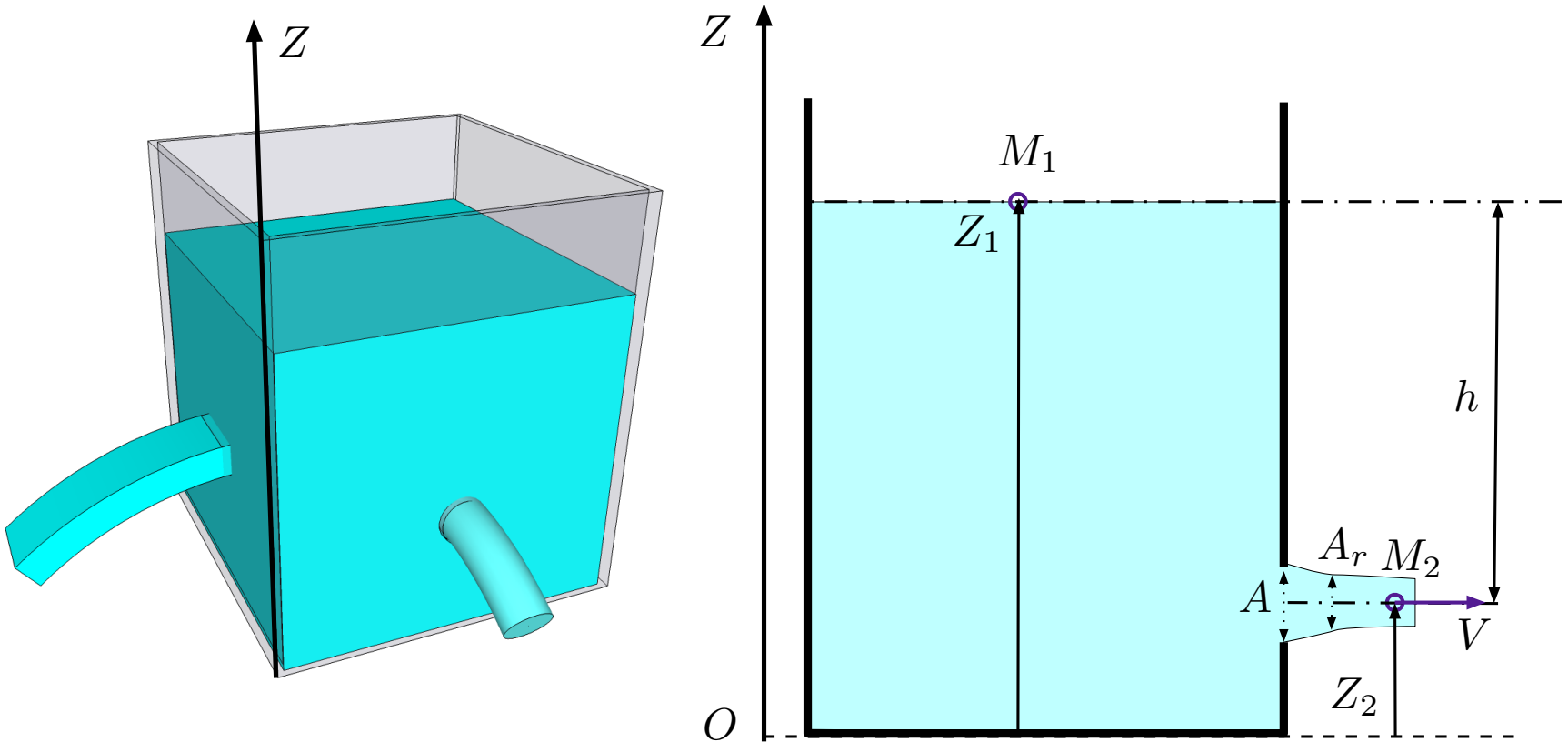


16. Point de fonctionnement



Débit théorique de Toricelli

$$H = \frac{P_a}{\rho g} + Z_1 = \frac{P_a}{\rho g} + Z_2 + \frac{V_{theo}^2}{2g} \Rightarrow V_{theo} = \sqrt{2gh}$$



Débit réel à travers un orifice

$$V = C_v V_{theo}$$

$$A_{contra} = C_a A$$

$$C_v \sim 0,98$$

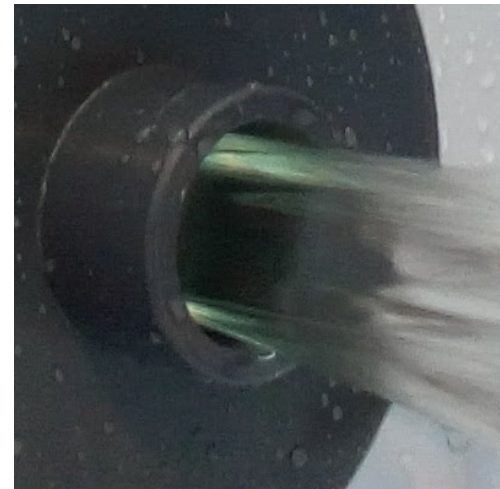
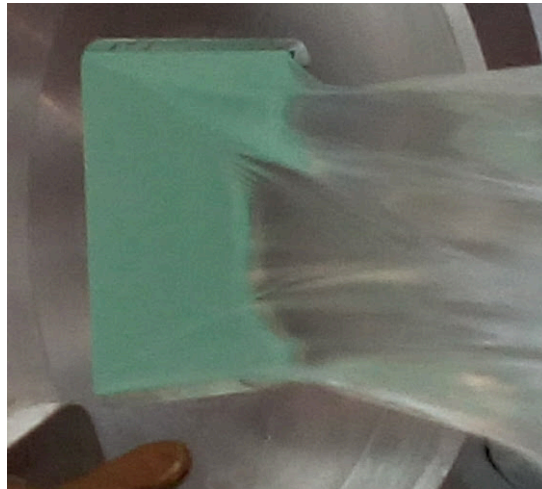
$$C_a \sim 0,60$$

$$Q = \mu A \sqrt{2 g h} \quad \text{avec} \quad \mu = C_a C_v = 0,59$$



Le coefficient correcteur dépend de la forme des orifices ou ajutages

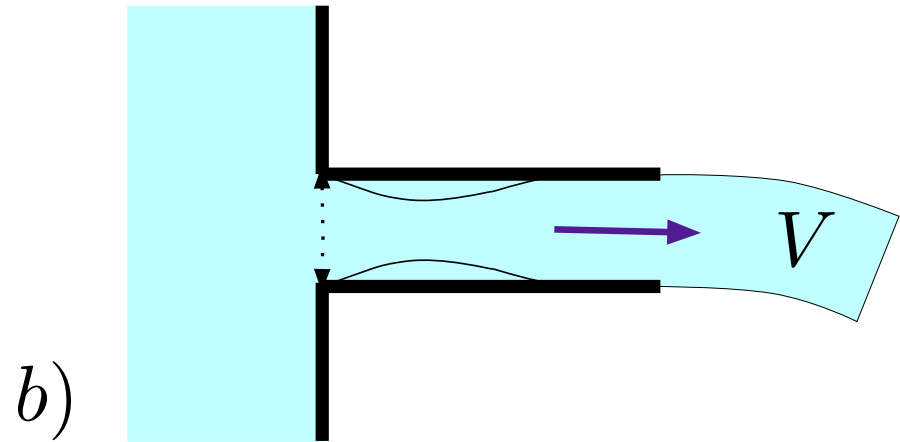
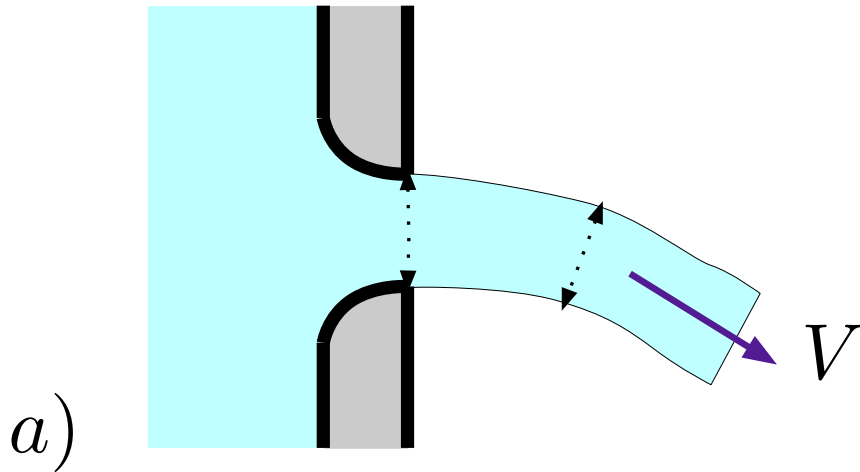
Orifices et ajutages



Coefficients correcteurs

Paroi moulée : $\mu = 0,96$

Ajutage : $\mu = 0,82$



Démonstration dans le cas d'un ajutage :

Perte de charge singulière : $h_s = K V^2 / (2 g)$ avec $K = 0,5$

$$h - h_s = V^2 / (2 g) \implies V = C_v \sqrt{2 g h} \quad \text{avec} \quad C_v = 1 / \sqrt{1,5} = 0,82$$

$$A_{contra} = A \implies \mu = C_v = 0,82$$

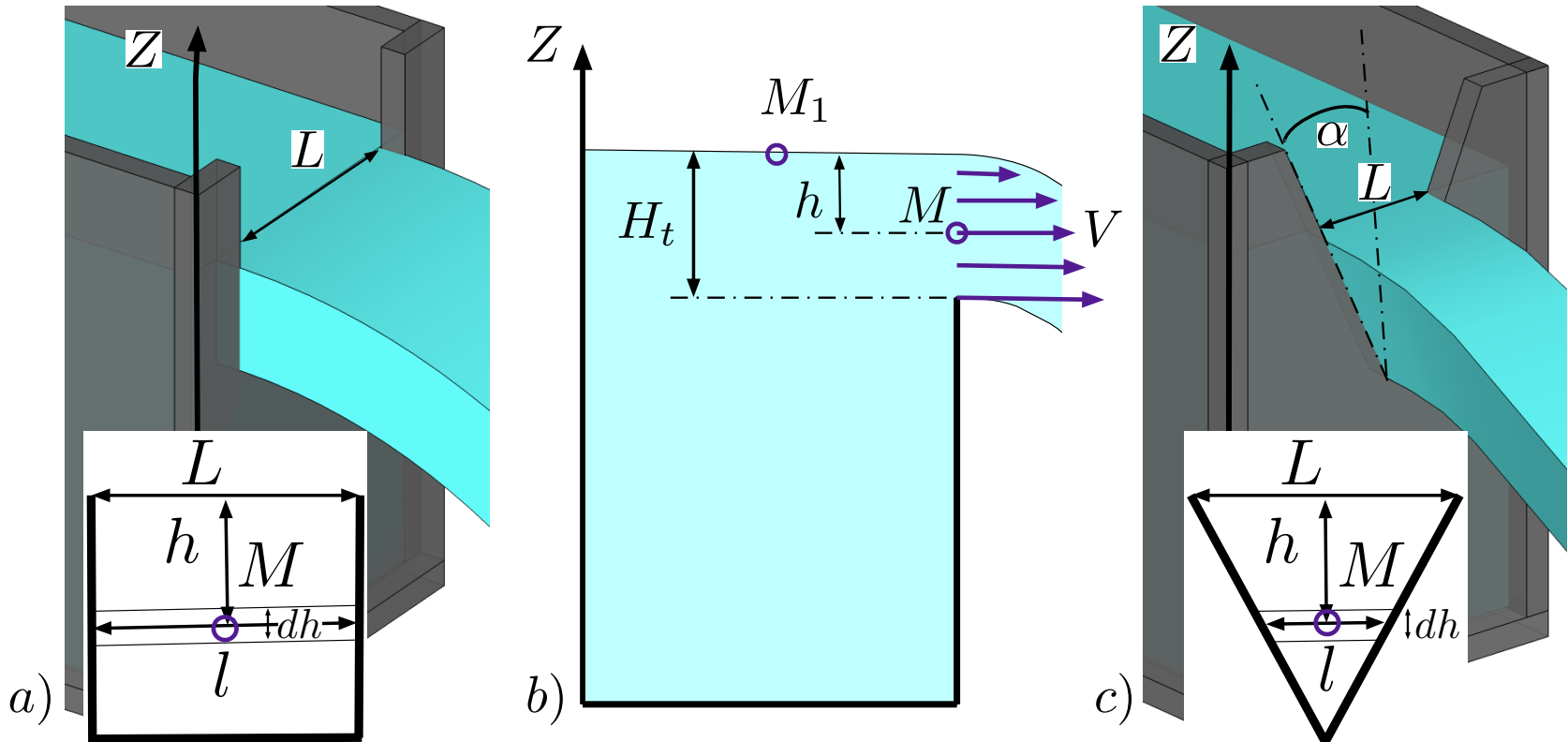
Débit à travers des déversoirs

$$Q_{rect} = \mu_{rect} L \sqrt{2g} H_t^{3/2}$$

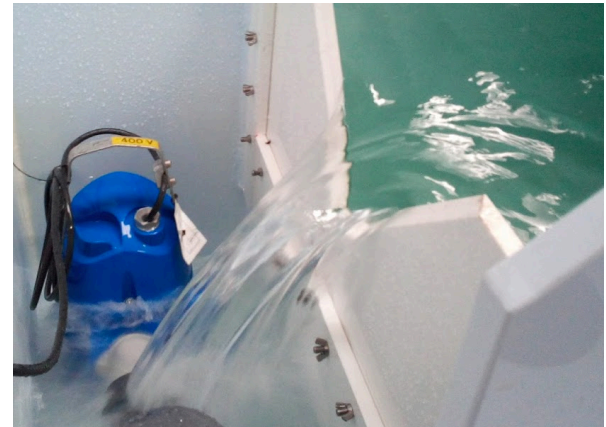
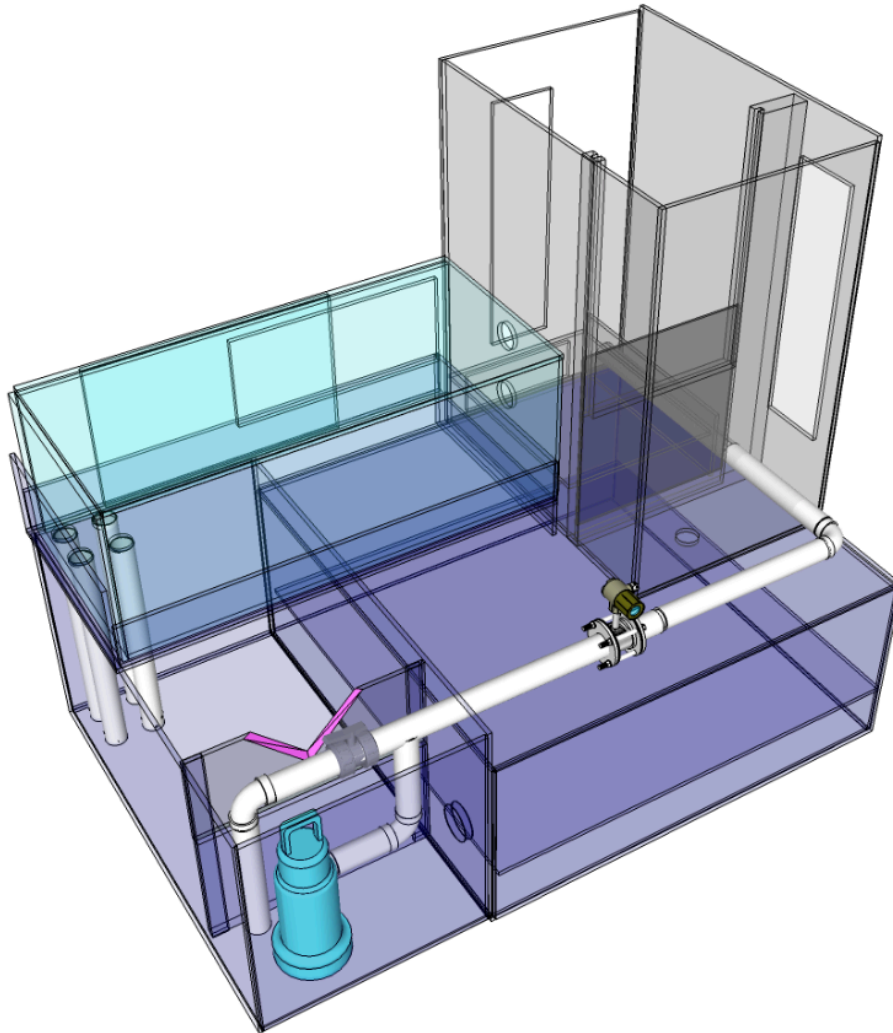
avec $\mu_{rect} = 0,415$

$$Q_{tria} = \mu_{tria} \frac{8}{15} \tan \alpha \sqrt{2g} H_t^{5/2}$$

avec $\mu_{tria} = 0,58$



Maquette orifices et ajutages



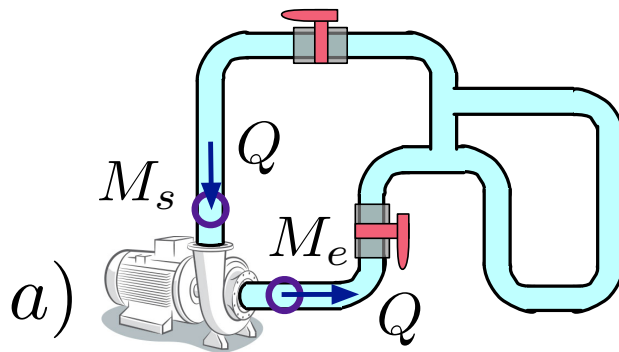
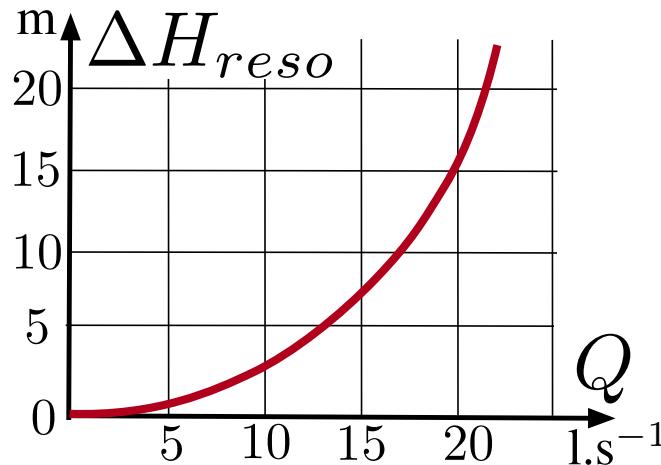
Courbe caractéristique d'un réseau

Réseau en charge

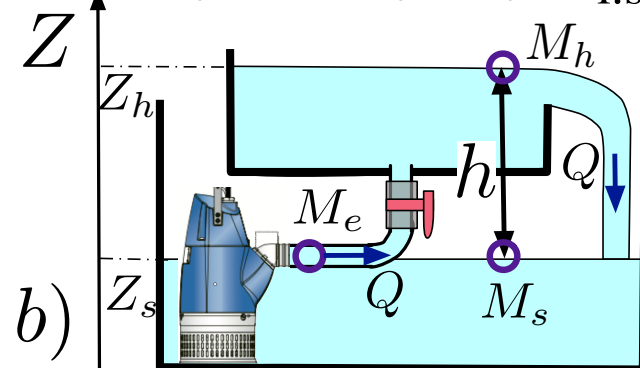
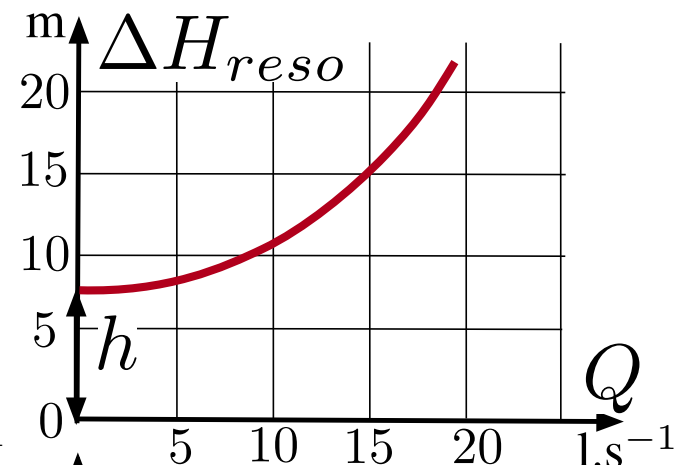
$$\Delta H_{reso} = H_e - H_s$$

Réseau avec surface libre

$$\Delta H_{reso} = h_f + h_s$$



$$\Delta H_{reso} = h_f + h_s + h$$

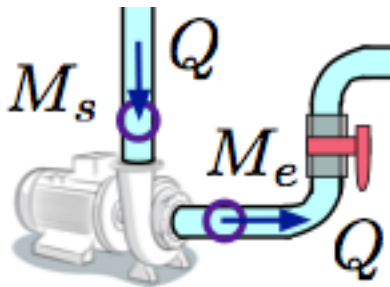


Courbe caractéristique d'une pompe

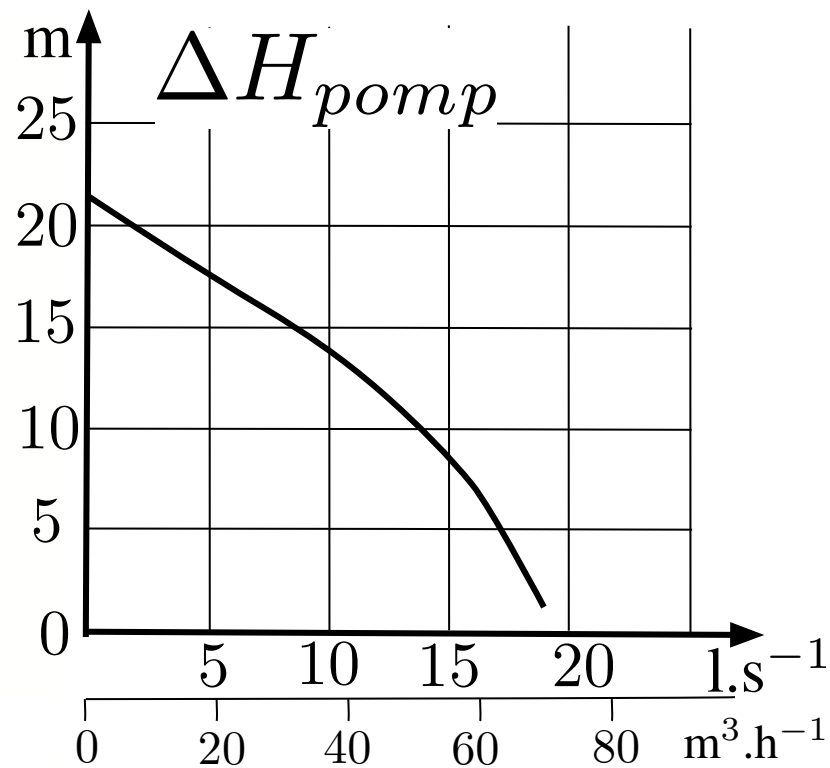
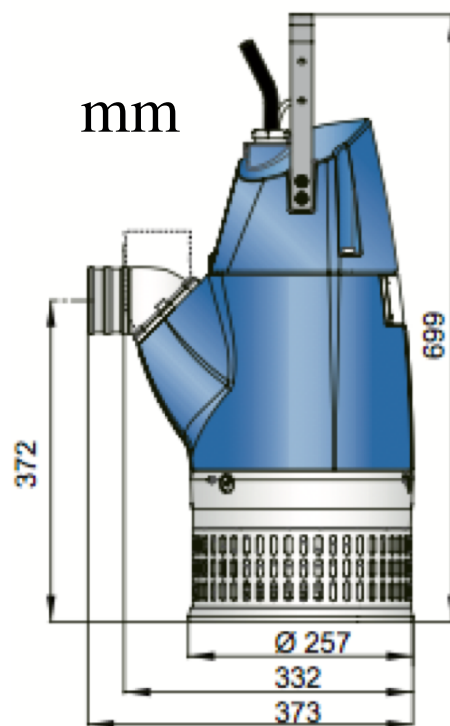
$$\Delta H_{pomp}(Q) = H_e - H_s$$

Hauteur de relèvement :

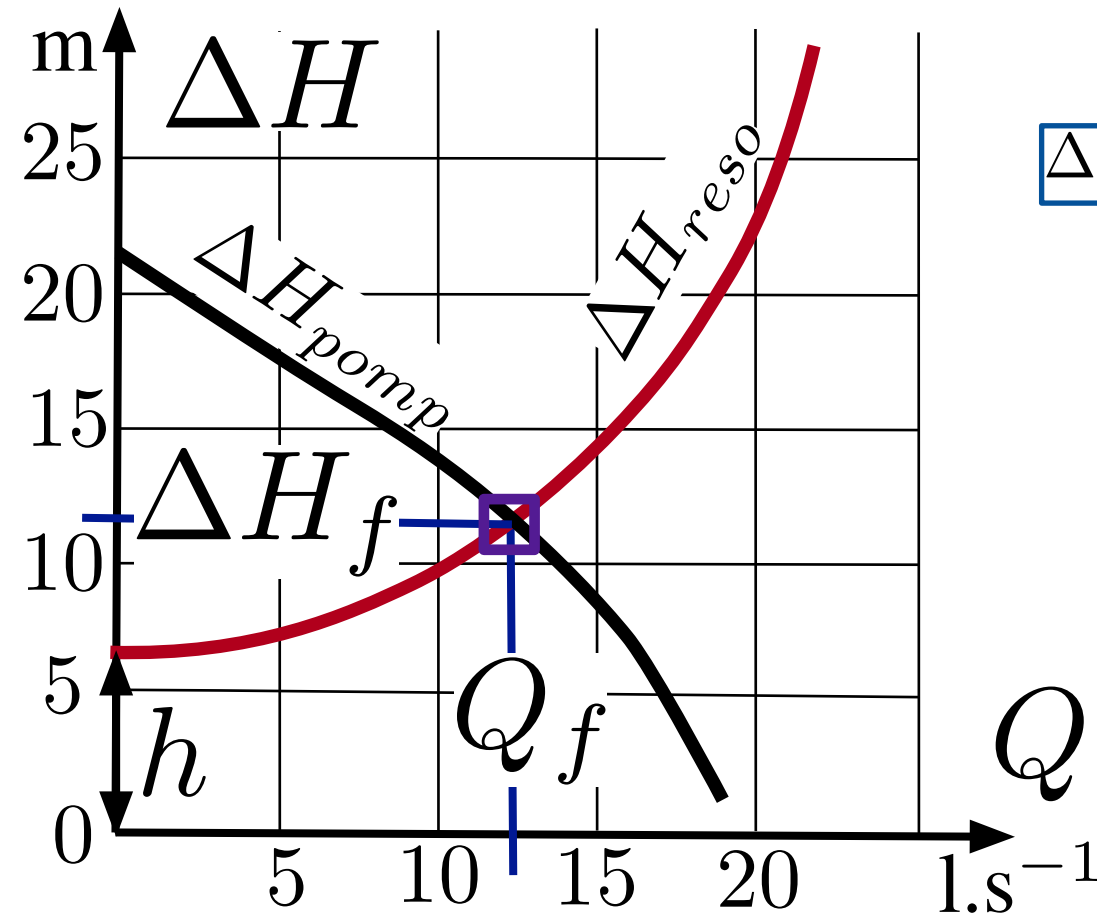
$$\Delta H_{pomp}(0)$$



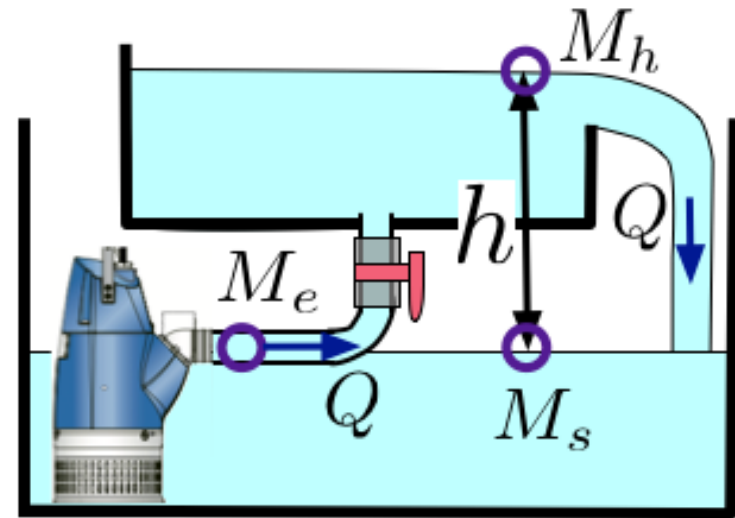
Pompe immergée
de la maquette
orifices et ajutages



Point de fonctionnement



$$\Delta H_{pomp}(Q_f) = \Delta H_{reso}(Q_f)$$

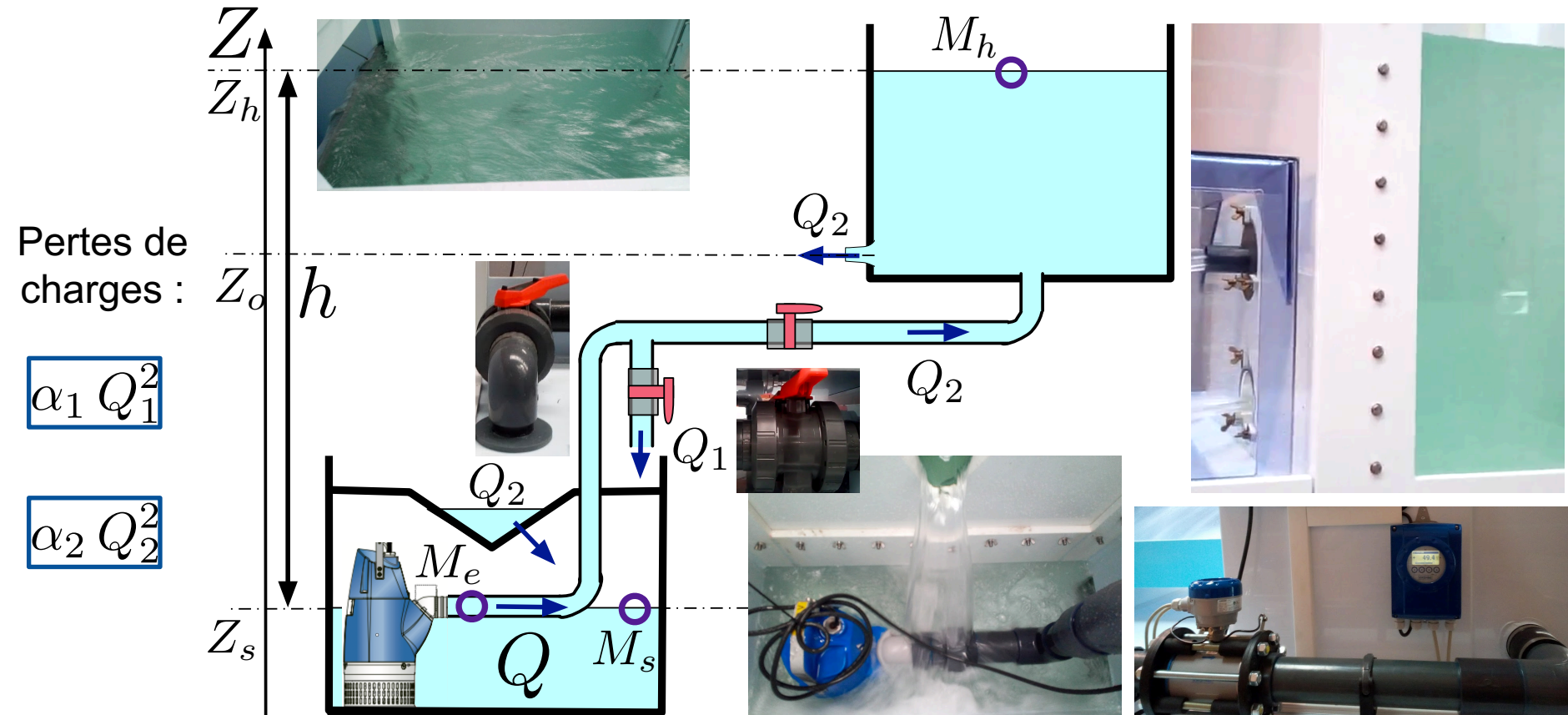


Exemple de réseau

$$h = Z_h - Z_s = 2 \text{ m}$$

$$Z_o - Z_s = 1 \text{ m}$$

$$\alpha = \pi/4$$



Calcul de débits

Modélisation de la pompe :

$$\Delta H_{pomp}(Q) = H_p [1 - (Q/Q_m)^2]$$

$$H_p = 20 \text{ m} \quad Q_m = 20 \text{ l/s}$$

Premier cas :

$$Q_1 = 0 \implies$$

$$Q_2 = 14 \text{ l/s}$$

Calculer : α_2

Deuxième cas :

$$Q_2 = 10 \text{ l/s}$$

Calculer : α_1

